

R&D Activities at the Laboratory of Sorption Processes

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Contents

- **Sustainable and reliable adsorptive machine**

Designing an efficient Adsorber/Desorber Plate Heat Exchanger (APHE)

- **Ohmic heating**

Experimental setup and first results

Contents

- **Sustainable and reliable adsorptive machine**

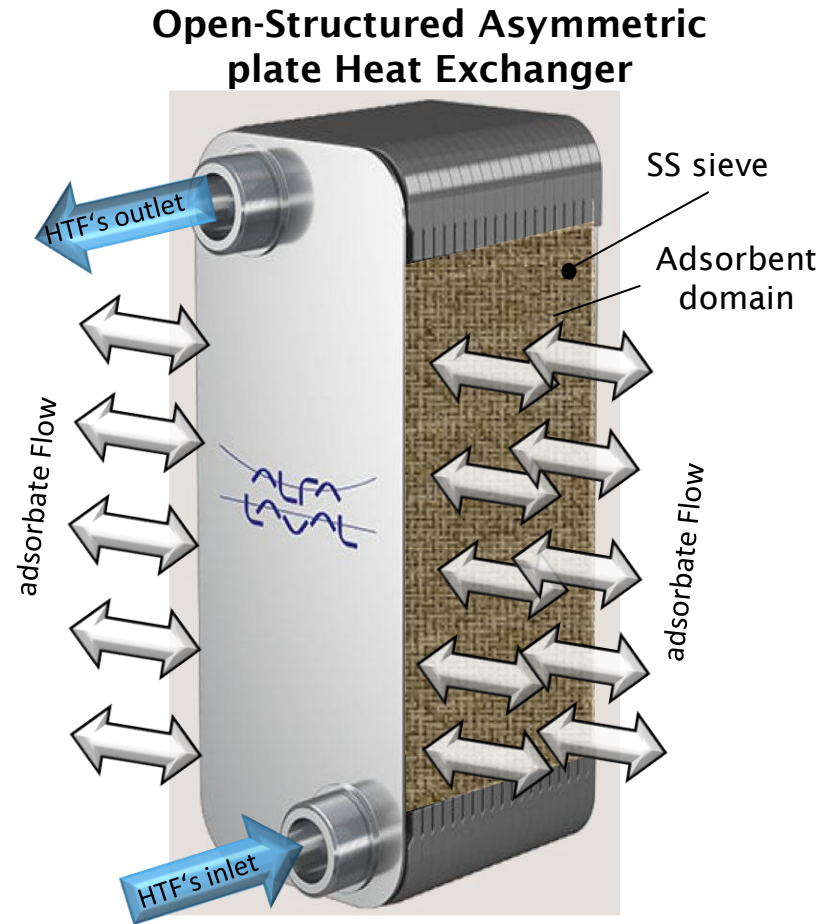
Designing an efficient Adsorber/Desorber Plate Heat Exchanger (APHE)

- Ohmic heating

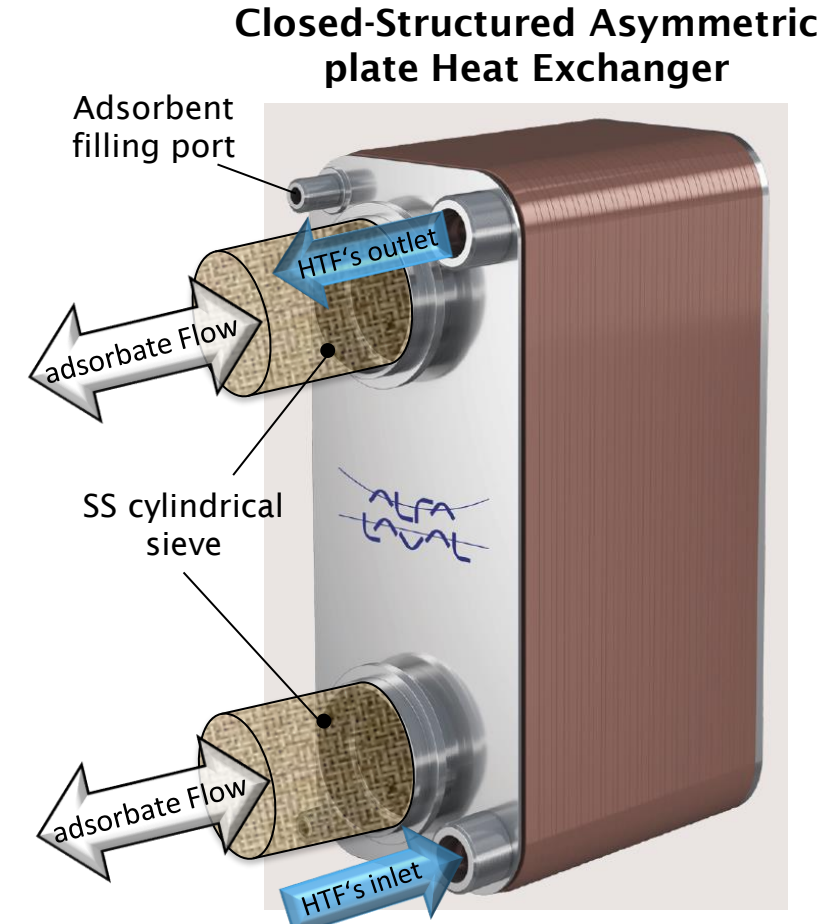
Experimental setup and first results

Tested Commercial Plate Heat Exchangers

- **G**as / **L**iquid plate heat exchangers
- Each Consists of stainless steel plates brazed together with nickel.
- Designed to handle asymmetric volume flows with exceptionally high performance.



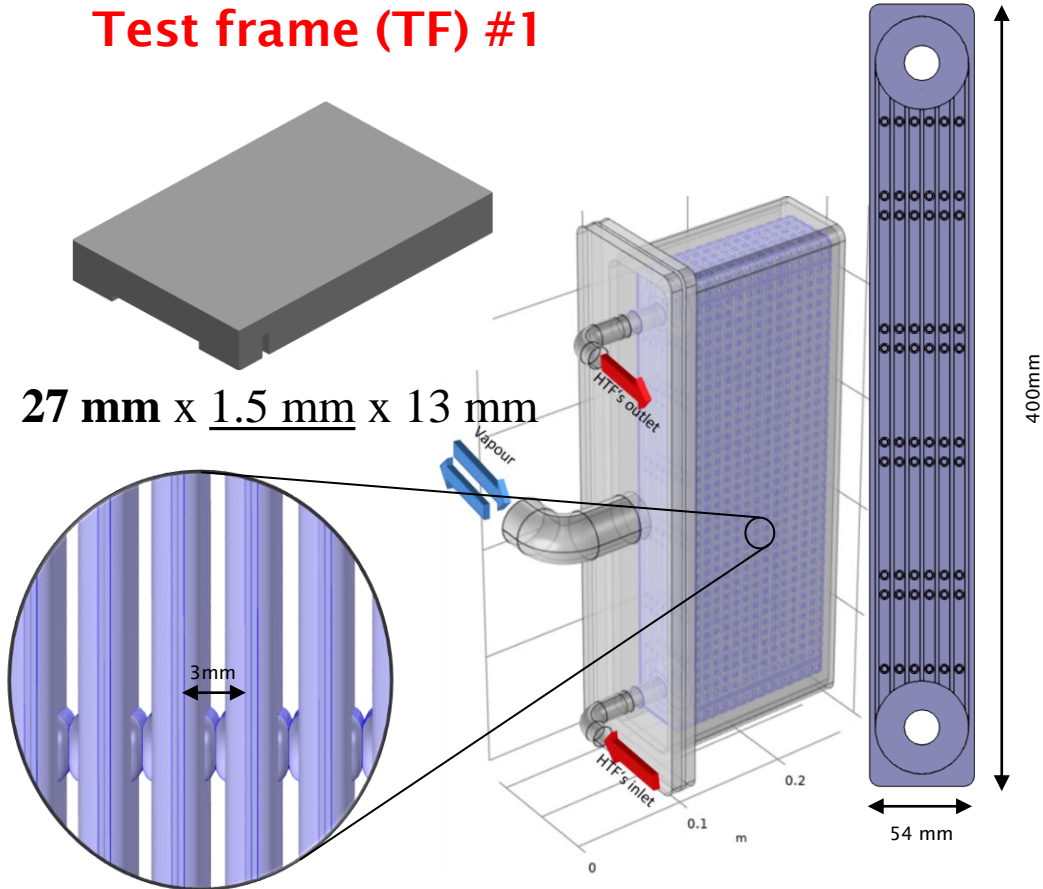
GLX30 PHE, AlfaLaval, Sweden



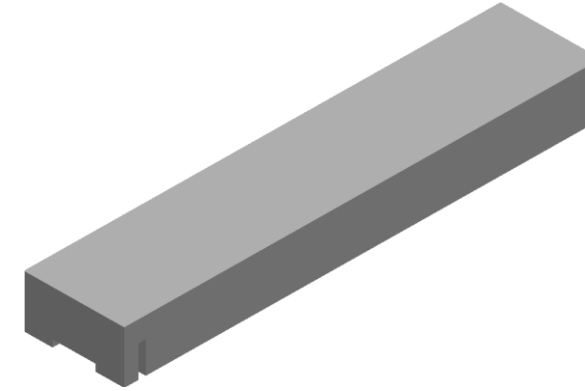
GL50 PHE, AlfaLaval, Sweden

Studying the effect of the heat and mass transfer characteristic lengths (HTCL&MTCL)

Test frame (TF) #1

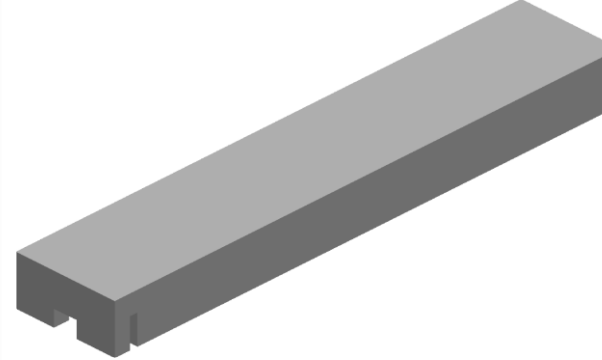


Test frame (TF) #2



58.5 mm x 1.5 mm x 6 mm

Test frame (TF) #3



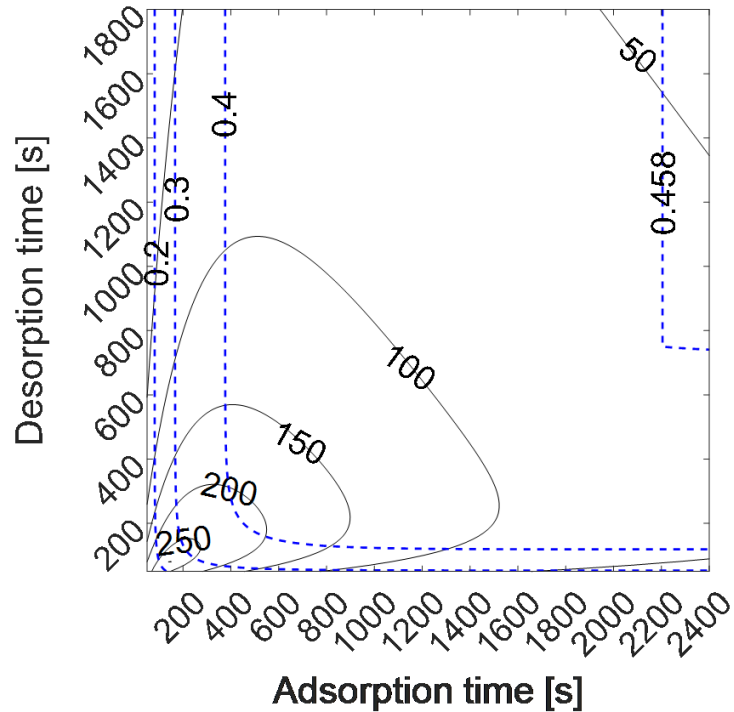
58.5 mm x 3 mm x 3 mm



GLX30 APHE

Mikhaeil, M., Gaderer, M., & Dawoud, B. (2020). On the development of an innovative adsorber plate heat exchanger for adsorption heat transformation processes; an experimental and numerical study. *Energy*, 207.

SCP - COP Chart



The **SCP** (black continuous lines) and **COP** (blue dashed lines) for the OTH APHE calculated at $T_{ev}=10^{\circ}\text{C}$, $T_{cond}= 35^{\circ}\text{C}$ and $T_{des}=90^{\circ}\text{C}$

Mikhaeil, M., Gaderer, M., and Dawoud, B. (2022). On the Application of Adsorber Plate Heat Exchangers in Thermally Driven Chillers; An Experimental and Analytical Study. *Appl. Thermal Eng.*, 220, 119713.

Comparison between the performance of the two investigated APHEs and an optimized finned tube adsorber plate heat exchanger at operating conditions of 10/35/90°C



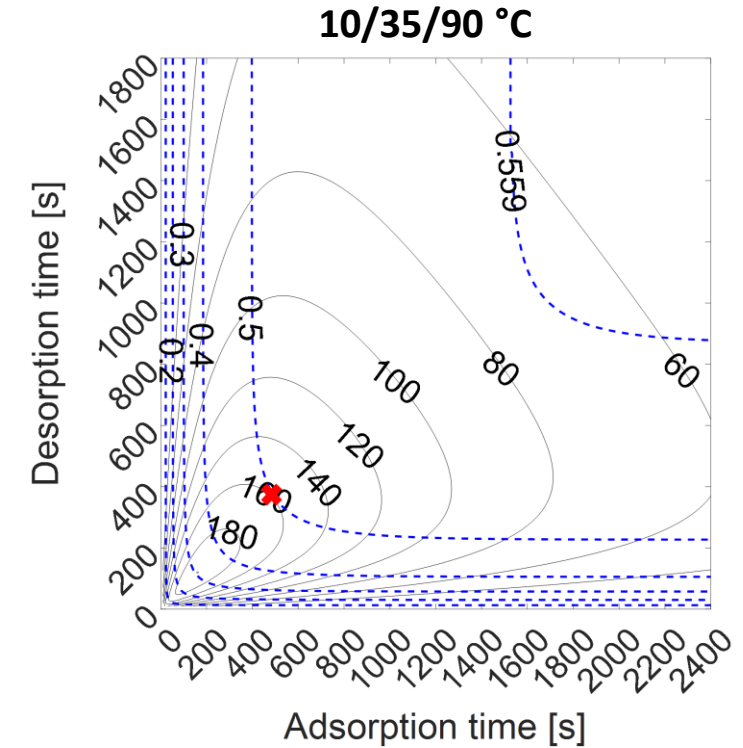
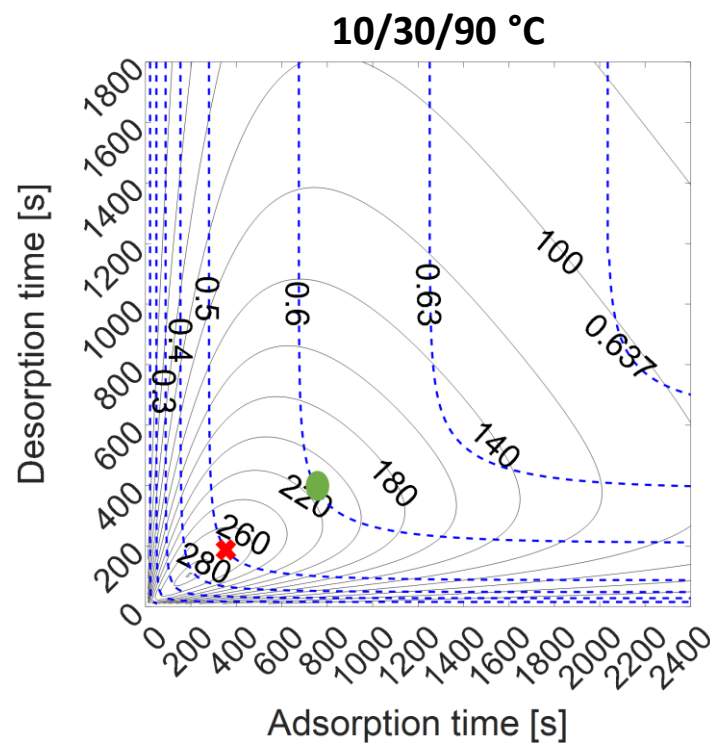
| | Newly Introduced APHE | GLX30 APHE | Finned tube adsorber heat exchanger |
|---|-----------------------|-------------------------|-------------------------------------|
| τ_{ads}, s | 257.7 | 586.1 | 243.5 |
| R^2 | 0.9957 | 0.9913 | 0.9908 |
| τ_{des}, s | 81.1 | 103.0 | 105.5 |
| R^2 | 0.9834 | 0.9813 | 0.9942 |
| Optimum t_{ads}, s and t_{des}, s | 150, 80 | 240,120 | 200, 125 |
| $SCP_{max}, \text{W}\cdot\text{kg}^{-1}$ | 263.6 | 131.9 | 268.0 |
| $COP_{SCP_{max}}$ | 0.242 | 0.147 | 0.51 |
| $SCP_{max}^*, \text{W}\cdot\text{kg}^{-1}$ | 308.6 | 154.5 | 268.0 |
| $COP_{SCP_{max}}^*, -$ | 0.271 | 0.168 | 0.51 |
| target $SCP^*, \text{W}\cdot\text{kg}^{-1}$ | 268.0 | 268.0 can't be realized | 268.0 |
| $COP_{target SCP^*}^*, -$ | 0.42 | | 0.51 |
| t_{ads}, s and t_{des}, s at target SCP^* | 380, 180 | | 200, 125 |

Optimized closed structured APHE

Specifications of the new APHE, designed for 10 kg of Siogel grains

| Specification | value |
|---|-------|
| HTF's inlet and outlet ports diameter (mm) | 18 |
| Thickness of one plate (mm) | 0.3 |
| Thickness of end plates (mm) | 2 |
| Number of plate-pairs, in case of gap between each two successive plate-pairs = 6 mm | 20 |
| Width of the PHE (mm) | 280 |
| Length of the PHE (mm) | 500 |
| Volume of the adsorbent domain (L), with gap between each two successive plate-pairs = 6 mm | 13.16 |
| Volume of the HTF domain (L) | 0.808 |
| Volume of the metal domain, with end plates (L) | 2.337 |

At 10/35/90°C operating conditions, the new closed-structured APHE provides 158.6W/kg at target COP of 0.5, while the open structured APHE of OTH could not achieve a COP higher than 0.458.



The SCP (black solid lines) and COP (blue dashed lines) calculated for the new APHE. The red cross symbols refer to the operating points at a COP target of 0.5. The green point refers to the operating points at a COP target of 0.6 at 10/30/90 °C

Contents

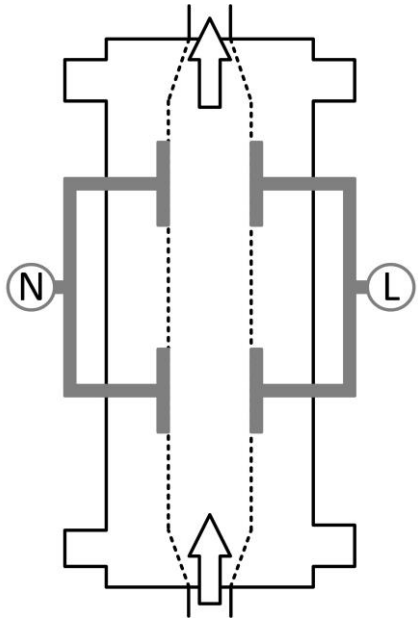
- Sustainable and reliable adsorptive machine

Designing an efficient Adsorber/Desorber Plate Heat Exchanger (APHE)

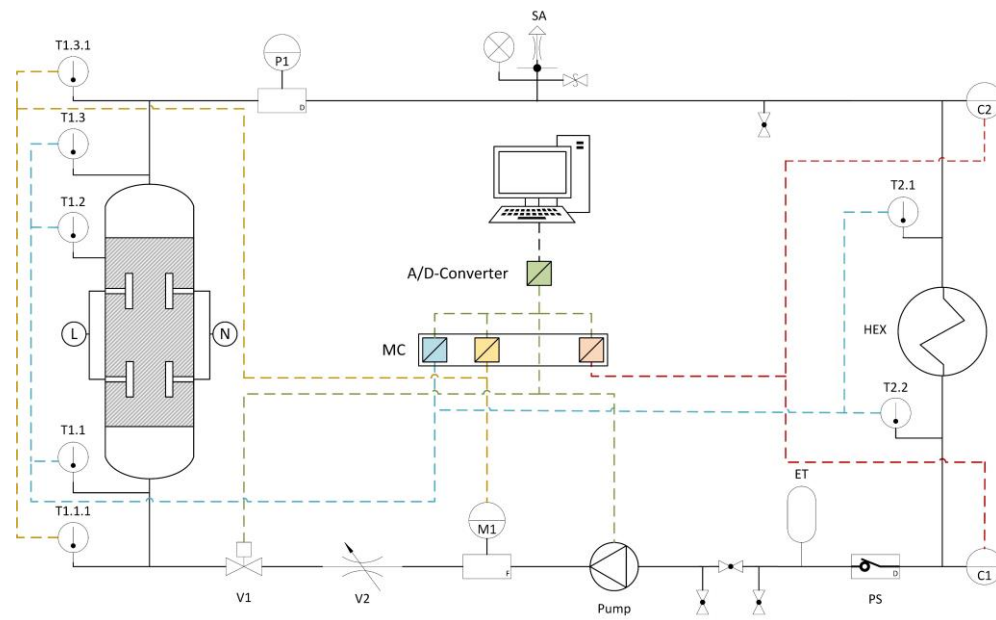
- Ohmic heating

Experimental setup and first results

Ohmic-Heating Setup



Scheme of the developed Ohmic-Heating Prototype based on the continuous ow principle.



Plant schematic with the main components, measuring and control devices and illustration of the communication with the central LabVIEW based measuring and control system.

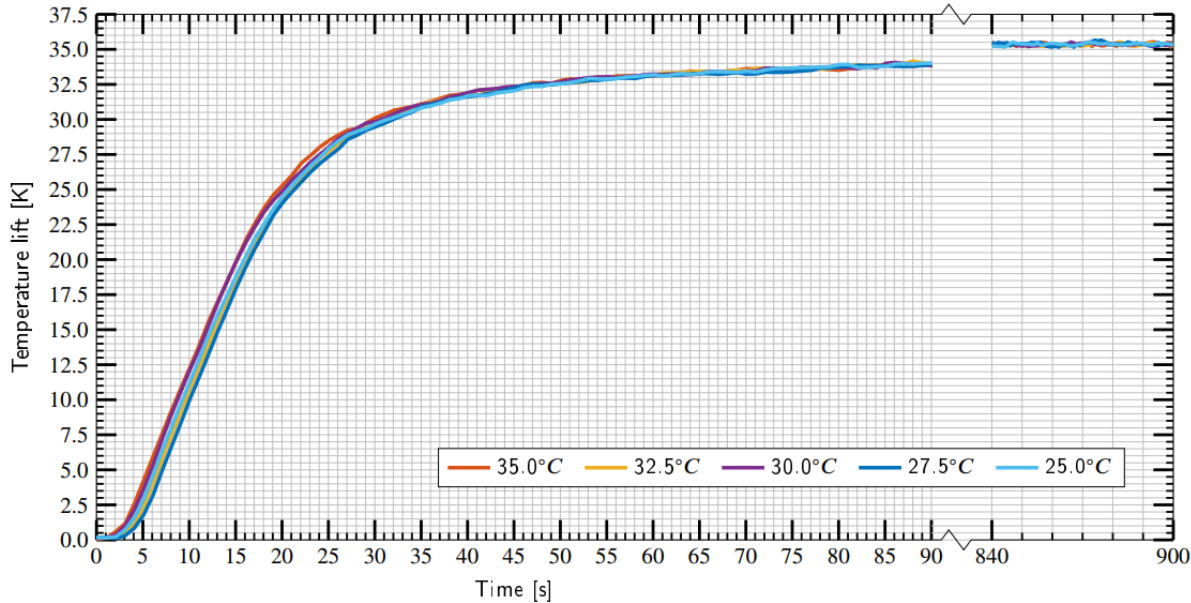


Photo of the laboratory test facility with the ohmic heating reactor, sensors and actuators and the electric boxes.

Ohmic-Heating: Working principle

Ohmic heating generates heat in the fluid itself. This is achieved by applying an **alternating current** across a **conductive fluid** with a specific electrical resistance, which results in a **direct conversion of the electrical energy into heat** through the generation of the so-called **joule energy**.

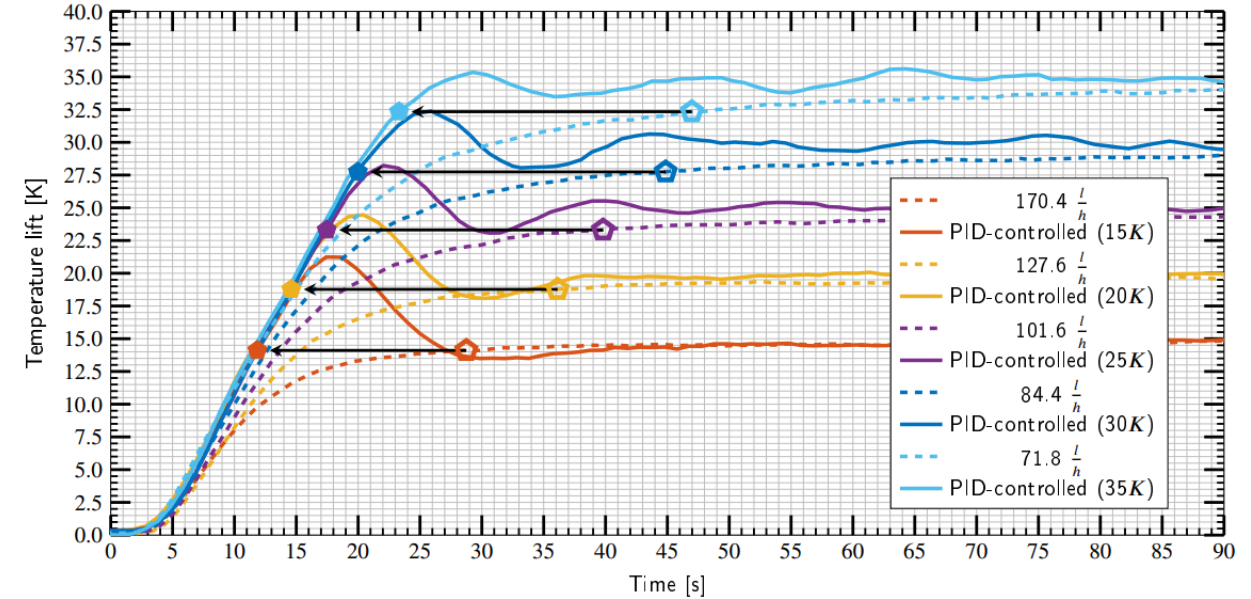
First results



Results a test mode exploring the dynamic thermal response of the ohmic heating reactor at a constant volume flow rate of 71.8 l/h and a step function of the electrical power of 3000W at the time 0 seconds at five different return temperatures

Key finding

Temperature lift is independent from return temperature with a measured conversion efficiency of $97.52\% \pm 0.16\%$



Test mode on the response time of the ohmic heating reactor at constant volume flow rates and a step function of the electrical power to 3000W at the time 0 seconds. Representation of five operating cases with different volume flow rates and corresponding stationary temperature lift in 5K steps from 15K to 35K. Marked time points of the RUT τ_{50} (triangle), τ_{80} (diamond) and τ_{95} (pentagon).

Key finding

Targeted temperature lift can be achieved in a very short time even with low electrical power

Future applications

Heating of LiBr-Solutions

Desalination of seawater

Organic synthesis in the chemical and pharmaceutical industry



**Thank you very much for your kind attention.
Questions are more than welcome!**